

RoPro 8-200 to 8-400

Installation Operation Maintenance Manual

**RoPro 8
Reverse Osmosis Systems
With OS3030 controller
With 8" membranes
With optional CIP tank & dosing pump output**

Models

8-200

8-250

8-300

8-400

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1.0 GENERAL NOTES

These instructions cover the RoPro Range of Commercial Reverse Osmosis System, which includes models with nominal outputs ranging from 240m³ to 480m³ per day.

It is recommended that these instructions are read throughout before commencing any work on the unit, particularly if you have no previous experience of installing and using a high pressure Reverse Osmosis System.

The instructions have been written in such a manner that the vast majority of the text applies to all the models in the range. However, in some cases, there are differences between different models, and when these result in a requirement to undertake a task in a different way, individual sections have been written to cover each case. These are clearly marked, and should be easy to identify.

Systems of this size will usually incorporate a number of custom additions required by the end user. This is generic manual and custom additions will be the subject of appendices added in at the end of the manual. If there are any additions, special attention should be paid to the appendices prior to installing the system.

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2.0 THE REVERSE OSMOSIS PROCESS

2.1 Introduction

Osmosis is a natural process involving fluid flow across a semi-permeable membrane barrier. It is the process by which nutrients feed the cells in our bodies and how water gets to the leaves at the top of trees.

If you separate a solution of salts from pure water using a basic thin semi-permeable membrane like a sausage skin, the pure water passes through the membrane and tries to dilute the salt solution. If the salt solution is connected to a vertical pipe then the progressively diluted solution will fill the pipe until the 'osmotic pressure' drawing the pure water through the membrane is the same as the head of solution.

This process can be reversed - hence 'Reverse Osmosis' - by applying a higher pressure to the salt solution. Pure water will then pass the other way through the membrane in a process that is easy to visualise as 'filtration' where the filter will only let through the small water molecules and retain almost all of the other molecules.

The mechanism of water and salt separation by reverse osmosis is not fully understood at the 'atomic' level. Current scientific thinking suggests two transport models: porosity and diffusion. That is, transport of water through the membrane may be through physical pores present in the membrane (porosity), or by diffusion from one bonding site to another within the membrane. The theory suggests that the chemical nature of the membrane is such that it will absorb and pass water preferentially to dissolved salts at the solid/liquid interface. This may occur by weak chemical bonding of the water to the membrane surface or by dissolution of the water within the membrane structure. Either way, a salt concentration gradient is formed across the solid/liquid interface. The chemical and physical nature of the membrane determines its ability to allow for preferential transport of solvent (water) over solute (salt ions).

2.2 Membrane construction

The semi-permeable membrane for reverse osmosis applications consists of a thin film of polymeric material a fraction of a millimetre thick cast on a fabric support. Commercial grade membranes have high water permeability and a high degree of semi-permeability; that is, the rate of water transport is much higher than the rate of transport of dissolved ions.

The membranes are stable over a wide range of pH and temperature, and have good mechanical integrity. The stability of these properties over a period of time at field conditions defines the commercially useful membrane life, which is in the range of 3 to 5 years. There are a number of different materials used for membranes and several ways of constructing them. This system uses Composite polyamide spiral wound membranes.

In a spiral wound configuration two flat sheets of membrane are separated with a permeate collector channel material to form a leaf. This assembly is sealed on three sides with the fourth side left open for permeate to exit. A feed/brine spacer material sheet is added to the leaf assembly.

A number of these assemblies or leaves are wound around a central plastic permeate tube. This tube is perforated to collect the permeate from the multiple leaf assemblies. The feed/brine flow through the element is a straight axial path from the

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feed end to the opposite brine end, running parallel to the membrane surface. The feed channel spacer induces turbulence and reduces concentration polarisation.

The spiral membrane is then enclosed by wrapping with glass reinforced resin into which is bonded an adapter cap at each end. The membrane is then housed in reinforced pressure tube with seals at each end. Water under pressure is introduced into one end of the housing/membrane assembly so that it runs between the feed channel spacer and the concentrate and permeate output piped away at the other

2.3 Pressure pump

In order to develop sufficient water pressure to overcome the Osmotic Pressure of the feed water and produce an acceptable volume of permeate, a three phase vertical multistage pump is used to boost the supply pressure by approximately 150 - 250 psi which results in the system running at 170-300 psi in normal service.

This type of pump is both quiet and reliable in continuous applications, requiring minimal maintenance with low energy costs.

2.4 Recirculation

Membranes will normally each 'recover' only 10-15% permeate from the raw water without fouling. However by returning a proportion of the concentrate exiting from the final membrane to the inlet of the pressure pump, the flow across the surface of the membrane is dramatically increased allowing a recovery ratio of up to 75% to be achieved without significant fouling. Recirculation also allows a higher flow of water through the pump, reducing the load on its bearings and helping the pump to run cooler. The recirculation rate on the RoPro Series is adjustable. On larger systems using a 'tapered array' recirculation is not required.

2.5 Recovery

The 'recovery' of a Reverse Osmosis System is a measure of the proportion of the total input water that is converted to high quality permeate. A recovery ratio of 10% means that only 1 part in ten of the input water is converted to permeate. At 50% recovery, half of the input water is converted. At 75% recovery, three quarters of the input water is converted to permeate.

The recovery ratio on the RoPro Series is adjustable, and its setting will affect the final water quality. At high recovery ratios, the amount of solids in the concentrate water as it exits the membrane will be high which will result in a higher level of solids in the permeate. However by reducing the recovery, the operating pressure in the system will also be reduced, which in turn can also result in a raised level of solids in the permeate since rejection rates are better at higher pressures.

A balance of the optimum water quality and volume is usually found at recovery ratios of 50%-65%.

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2.6 Rejection

The rejection ratio is a measure of the amount of solids dissolved in the raw water that are 'rejected' by the membrane. A rejection rate of 99% means that only 1% of the dissolved solids will pass through the membrane, and these are usually of low molecular weight.

At 99% rejection on a raw water supply of 400 ppm, you would therefore expect a permeate quality of 4 ppm. However by running single membranes at high recovery levels with considerable recirculation will mean that the membrane actually 'sees' a raw water of 1000-1500 ppm which could give a product water quality of 10-15 ppm. This is still a very pure water, but may need additional polishing through a mixed bed ion exchange resin if ultra-low TDS water is needed for process.

2.7 Flush

In order to remove fouling that accumulates during service it is essential to periodically flush the membrane at a high water flow.

The controller fitted will automatically flush the membrane at the end of a production run and also flush it periodically during standby.

2.8 Pre-Treatment

For a Reverse Osmosis plant to function as efficiently as possible, the raw water feeding the system needs to have its hardness reduced by a water softener, or inhibited with special chemicals that are dosed in to the supply upstream of the system. For small industrial R/O systems like the PC Series, duty/standby duplex softening is preferred since it is very cost effective and contributes to the longevity of the membranes.

The Composite Polyamide membranes used in high output Reverse Osmosis systems do not tolerate high levels of Chlorine. This should be removed with a backwashing filter filled with Granular Activated Carbon.

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3.0 UNPACKING AND IDENTIFICATION

3.1 Basic Packages

The Reverse Osmosis unit will normally be delivered as a single item on a wheeled frame with locking castors. Additional items may also be supplied if ordered, such as a product water storage tank, pre-filter or water softener. If no additional items have been ordered, then a set of level probes will also be supplied for installation in to the customer's treated water storage tank.

3.2 Unpacking notes

The unpacking of system is straightforward and there are no 'hidden' items. It is advisable to keep the system with any external wrapping complete until ready to complete installation to prevent dust or water ingress.

Care must be taken if carton slitters or hobby knives are used to remove any external wrapping since there are control cables and high pressure hoses routed around the system frame.

3.3 Lifting

Caution: The R/O system will weigh between 600 and 1200 kg depending on the model. The frame is fitted with wheels so that the system can easily be pushed into place then the castors locked so that the system will not move.

If the system must be lifted clear of the ground, suitable lifting straps must be used which will lift the system by the base without stressing components on the frame

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4.0 Temporary Storage

If installation is not to start immediately after delivery, the equipment should be stored in a clean dry area, where it will not be damaged, or be subjected to temperatures below freezing.

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5.0 DESCRIPTION OF SYSTEM

Stainless steel frame with two or more multiple membrane pressure vessels fitted with ESPA membranes, electronic controller, flow meters, valves, sediment filter, vertical multistage pressure pump and all interconnecting pipe work.

The inlet connection point is positioned on right of the system feeding the sediment filter housing. There is an raw water pressure gauge point on the inlet filter manifold. After the filter is the inlet valve and then pipework takes the supply water to a manifold on the inlet of the pressure pump. On this manifold is the low pressure switch, inlet pressure gauge line, recirculation return and piping to the CIP cleaning tank outlet port if fitted.

The control panel will not initiate service unless the water pressure is above the minimum set, currently 1.0 bar. This level is set low since the high pressure pump draws water at a very high rate during flushing with the effect that the monitored inlet pressure will drop.

From the pump, high pressure water is piped via a manifold to the inlet on the end of the first, lowest membrane housing. The manifold is also fitted with a high pressure cut out and pump pressure gauge line.

The permeate outlet from each housing is connected to the inlet of the permeate flow meter. The outlet of the permeate flow meter is terminated with a 1.1/2" or larger ball valve. In addition there is a tee on the permeate line with a 1.1/2" ball valve which can be used during cleaning to return permeate to the CIP tank if fitted.

The concentrate outlet from the lower membrane housing or array is connected to the inlet of the next membrane housing or stage (if fitted). Subsequent membranes continue this sequence. The inter-housing pressure is also monitored.

The concentrate outlet from the final membrane is piped to a manifold with an adjustable recirculation flow controller, pressure gauge line, tee to the flush line and a pressure regulating/concentrate valve. The regulating valves are used to control the back pressure in the concentrate line and the recirculation flow. On the concentrate line there is a 1" high pressure ball valve fitted which can be used during cleaning to return concentrate to the CIP tank if fitted.

The recirculation valve directs a proportion of the concentrate water back to the inlet of the high pressure pump which maintains the water speed over the surface of the membrane. Water is recirculated to help give high recovery of permeate from the concentrate water, and also to keep up the flow across the surface of the membrane to prevent fouling

The flows have been factory tested under working conditions, but the concentrate valve has been opened prior to despatch in order to fill the membranes with preservative. The valve will need setting up on site to balance the outputs to the user's requirements depending on the incoming water pressure and quality.

Pressure gauges supplied are glycerine filled to minimise bounce and prolong the service life.

If a permeate storage tank has not been ordered, a tank 'full/restart' level sensor and flying lead has been included with the system to be installed in the permeate tank. Installation will require the tank cable to be connected via the tank connector/stuffing assembly the two core flex and two way connector to the Reverse Osmosis system.

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6.0 PRE INSTALLATION CHECKS

6.1 MECHANICAL

6.1.1 Foundations/Drainage

The Reverse Osmosis unit and pre-filter will not require any special foundations, provided that a firm, level area which is capable of supporting the working weight (see Engineering Data, **Section 12.2**) is available.

Reject/concentrate water from the process must flow to drain, or to a storage tank where it can be utilised for other processes that do not require high quality water such as washdown or lavatories.

If the system is simply run to waste this must be to an open drain or gully, capable of passing the necessary flow is required (see Process and Operating Data, **Section 12.1**, for relevant flows). The total flow of water to drain depends on site conditions, but will typically be between 50-100% of the product water flow. The drain must not be at a level higher than the Reverse Osmosis unit and preferably should be installed with an air break at the same height as the drain outlet.

6.1.2 Operating Space

It is difficult to be precise with regard to the floor space which will be occupied by the assembled unit, since there will usually be associated pre-treatment and product water storage. However, an idea can be gained from reference to the Engineering Data (**Section 12.2**).

Access will be required to monitor the operating pressures, permeate & concentrate flows, and permeate conductivity. Access will also be needed to carry out adjustments or maintenance on the equipment. It is therefore recommended that a minimum of 500mm clearance be allowed around the base for this purpose.

Since the system is wheeled, it can be easily moved to allow replacement of membranes.

6.1.3 Incoming Water

The raw water to be fed to the Reverse Osmosis GAC pre-filter unit must comply with the following:

- (a) Available at all times at a flow equal to the required maximum service flow or greater.
- (b) At a pressure between 2.0 and 5.0 bar at the service flow required.
- (c) Temperature between 10°C and 40°C.
- (d) Iron less than 0.2 ppm, Manganese less than 0.1ppm.
- (e) Free Chlorine less than 0.2 ppm
- (f) Softened to no greater than 10ppm hardness as CaCO₃ or dosed with a suitable and approved antiscalent .

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6.1.4 Pipework

Pipework to be connected to the Reverse Osmosis Unit should not have an excessive amount of Iron or hardness scale deposit. Piping that is heavily built up with scale or Iron deposits should be replaced.

Make sure that the pipework can be connected to the Reverse Osmosis Unit in such a way as to impose no stresses on the inlet connection, and that it is properly aligned and supported. Excessive vibration can cause erratic operation of the valve valves, so, if required, a suitable vibration damper should also be installed. Final connections to the Unit should be made where possible using flexible connections to avoid stresses during operational cycles.

6.1.5 Water Supply Company Requirements

It is essential that the equipment is connected to a pressurised water supply. If connected to a mains supply the local bye laws must be adhered to. These cover both plumbing and the prevention of back flow into the mains. If there is any doubt, the local water inspector should be consulted, but in general, the installation of a 'Double check valve assembly' conforming to BS.6282 part 2 will be required in the supply pipework to the system, or a suitable break tank and pressure booster pump.

6.2 ELECTRICAL

The system requires a continuous three phase supply of 415v, 50 Hz with a rating as indicated in Section 12.3. A soft starter, contactor and overload is fitted in the transformer enclosure on the frame. A isolating switch and MCB should be installed on an adjacent wall to supply the system.

A continuous three single phase supply of 24v, 50 Hz with a rating of 5 Amps is required by the Reverse Osmosis Unit controller. A 240/24v fused safety isolating transformer is fitted to the frame to provide power to the controller with its supply taken from one of the inlet phases.

A 240v dosing pump supply connection is fitted to the transformer enclosure which is powered during the normal run and flush cycles of the system. The dosing pump connection is not powered during the manual maintenance cycle.

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7.0 INSTALLATION

7.1 MECHANICAL

Flow diagrams showing the suggested overall layout of the system is included in Section 14 ,and should be referred to for guidance.

Check all the items against the parts list and shipping documents, and ensure you have them all before starting work. In addition to the components you will require basic tools, (i.e. spanners, screwdrivers etc., and P.T.F.E. tape).

7.1.1 Inlet Pipework

Pipework should be assembled incorporating the features shown in the Flow diagrams, Section 14. It is essential that an inlet isolating valve is provided, and that the water main is protected by a double check valve where appropriate (see Local Water Bye laws).

Pipework can be constructed from any normally acceptable material (Copper, Galvanised, Plastic), provided it is properly supported and aligned. Ensure that the pipe is sufficiently large to accommodate the flow of water required.

NOTE: IF BRAZED OR SOLDERED FITTINGS ARE TO BE USED, THE PIPEWORK MUST BE DISCONNECTED FROM THE SYSTEM CONNECTIONS DURING HEATING AND COOLING. EXCESS HEAT CAN CAUSE PERMANENT DAMAGE TO SOME OF THE SYSTEM COMPONENTS.

The inlet pipework should be connected to the inlet port on the filter housing manifold.

7.1.2 Drain Connection

The R/O drain pipework should be connected to the ball valve outlet from the concentrate flow gauge

The concentrate should be run to a drain or concentrate storage tank capable of taking the maximum flow during flushing (see **Section 12.1**), using flexible tube it at all possible. An air gap is necessary on the drain line from the system to prevent negative pressures acting on the membrane.

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7.1.3 Permeate Connection

The permeate connection is made to the ball valve on the outlet from the permeate flow meter and should be made with piping of at least the same bore as the permeate line. There is also a ball valve on the permeate line for use during membrane cleaning.

Install a suitable overflow in the permeate storage tank. This must be below the level of the permeate inlet and must also make allowance for permeate production during flushing (**see Section 7.2.3 & Drawing Section 14**)

The top of the permeate storage tank should be no higher than 500mm above the outlet fitting on the top of the membrane to prevent operating back pressure on the membrane during production or static pressure on the membrane during standby. Back pressure during production reduces the output of the system. Static pressure on the membrane from a column of water can de-laminate the membranes during standby.

The permeate inlet to the tank must be open with no restriction. Under no circumstances must a float shut off valve be used to close off the permeate delivery line.

The permeate inlet must be at least 100 mm above the overflow/high water level in the storage tank to prevent permeate being drawn back through the membrane by osmosis during standby.

Prior to making the permeate connection final, make a temporary pipe connection from the permeate outlet or cleaning port to drain so that the system can be fully flushed during commissioning.

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7.2 ELECTRICAL

Electrical installation is very straightforward, but should still be carried out by a competent electrician, and must conform to the appropriate standards of safety.

7.2.1 Mains Supply

The mains supply connection should be made through separate, switched supply, fused and earthed in accordance with Institute of Electrical Engineers Regulations.

One power supply is required by the system. This should be 415v, 50 Hz three phase supply plus neutral and earth, with an isolator and MCB rated as detailed in the data sheet in Section 12.3.

The power supply for a 24v AC pre-filter or softener is provided by the system control panel via terminals 1&2 in a plug in 6 way connector that mates to a socket on the side of the transformer enclosure.

7.2.2 Auxiliary closedown

There is a low voltage interlock between the R/O controller and the softener/filter valve. This ensure that the R/O shuts down while the filter is regenerating.

The feedback/shutdown cable between the softener or filter valve and the R/O controller is joined using the using same plug in connector that provides power to the valve. The feedback line uses terminals 3&4

7.2.3 Level sensor installation

Install the level switch on the treated water storage tank. This may require the cabling to be disconnected at the 2 way plug on the end and the terminals re-made when the probes have been installed. The blue and brown wires run from terminals A and C in the sensor and are connected to the terminals L & N in the 2 way connector which plugs into the transformer enclosure on the back of the R/O unit.

The floats for the sensor will need to be tied to hook on the underside of the sensor using the rod proof string provided. When the second float is tied to the bottom of the first float, the R/O unit will switch off when the level reaches the middle of the upper float, and will turn on again when the level drops to the middle of the lower float. This mean that the highest practical treated water level in the storage tank is 150mm from the top and the minimum differential is 170mm

Important: When installing the level sensor in the permeate tank, the middle of the top float must be at least 100 mm below the overflow since permeate will flow to the tank during the post-service flush.

7.2.4 BMS/Alarm connection

The controller has an integral volt free alarm contact that can be utilised to connect in to a BMS system. See controller wiring diagram in Section 14.3.

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8.0 COMMISSIONING

The GAC filter will need to be filled with water and flushed prior to supplying dechlorinated water to the R/O system. The R/O membrane(s) are shipped in preservative which will also need to be flushed prior to putting permeate water to service. Commissioning and flushing should take place immediately before the system is put into service

8.1 Pre Service Flush

8.1.1 Pre-filter system

Commission and flush the pre-filter system prior to opening the valves to the R/O unit.

8.1.2 Reverse Osmosis Unit

Remove the cover on the transformer/contacter enclosure ensure that the pump starter is set to This will disable the pump contactor.

Turn on the main power supply.

Turn on the R/O controller with the rocker switch under the outer cover.

The controller should default to Service, but if it does not then press the service button.

The inlet valve will then open allowing water to flush through the system but the pump will not operate since its contactor is disabled.

Open the pressure regulator by unscrewing the valve handle knob five full turns. Leave the system like this for 5-10 minutes in order to prime the pump, fill up the membrane housings and start primary flushing. Open the pump priming plug until all air is vented from the pump.

If the system cuts out at this point because of high permeate TDS, reset the maximum threshold or temporarily disable the cut-out (see OS3030 instruction manual) and continue.

Check for leaks with low pressure running in the system.

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8.2 Pressure flush

Prior to closing the motor starter isolator terminal, wind in the pressure regulator knob until it stops then back it off at least six turns. Switch off the mains power, close the motor contactor isolator terminal, and turn on the power supply. Ensure that the control panel is still indicating Service.

The inlet valve will open, then after a short delay the pump will power up and the system will run up to pressure after a primary flush. The system has a soft starter installed to reduce the starting load on the power supply and water hammer in the system. The pump motor will start initially at low speed then after 3-10 seconds will cut in to full power.

Check the direction of rotation of the pump is correct. If it is not, shut the system down immediately and reverse the yellow and blue two phase connections to the system.

Monitor the permeate and concentrate flows and balance with the pressure regulator so that the permeate flow is approximately the same as the concentrate flow (50% recovery) or as otherwise required.

This should give a back pressure on the pump (centre) pressure gauge of 170-300 psi depending on the raw water pressure.

Do not adjust the concentrate valve so that the pump pressure exceeds 300 psi.

Leave to run to drain for 30-60 minutes to flush the preservative out of the membranes. During the flush period, monitor the concentrate flow and fine tune to no more than 75% recovery (concentrate 1/3 of permeate).

If the permeate is then to the correct quality then the system can be put into service.

8.3 Service connections and checks

With the system switched off, connect the permeate tube to the storage tank. Turn the system on and leave to run to service.

Test the flush circuitry by lifting both tank switch floats. This will initiate a 'post service' flush. The pressure pump will cut out as the float switch is operated. Shortly afterwards the flush valve will open and then the pump will start up again. This will flush the membranes at a high flow rate for the time set in the controller. Lowering the floats will immediately switch the system back to service.

If the pump draws a massive amount of water during flushing it may be necessary to adjust down the low pressure threshold. Monitor the inlet pressure during flushing on the top pressure gauge

During normal production, there should be no more than 2.6 bar (40 psi) pressure difference between the feed pressure off the pump (centre gauge) and the back pressure on the membrane (bottom gauge).

The system is now commissioned.

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9.0 Operation

The RoPro Reverse Osmosis systems are designed to run and flush automatically and should not be turned off at the mains after a production run of permeate.

For the first few days of use, the operating pressures, permeate and concentrate flows should be monitored every few hours and the system fine tuned as the membrane settles down to its working environment.

Thereafter the flows, pressure and permeate conductivity should be monitored daily at a regular time when production is taking place. These readings will vary slightly due to variations in incoming water temperature and pressure. An example data recording sheet can be found in section 9.3

If a variation of more than 15% is noted in the permeate flow at usual operating pressures then the system should be cleaned with an appropriate recirculating cleaner. This must be done by a service technician with a thorough understanding of reverse osmosis systems and their cleaning regimes

9.1 Routine maintenance.

Daily Monitor permeate and concentrate flow, inlet, pump and back pressures, and product water conductivity.

Weekly Monitor raw water temperature

Monthly Inspect system for leaks and tighten fittings where necessary

3 Monthly Replace inlet filter cartridge

Annually Clean membrane with a recirculating cleaner if normalised output has fallen by greater than 15%

Bi-Annually Service GAC filter valve and replace media

9.2 Temporary Shutdown

If permeate is not required for up to five days then the system should be left with the permeate tank empty, the level probes disconnected and the water and power supplies turned on. The controller will automatically flush the system every 24 hours and a small amount of permeate will flow to the tank.

If the permeate tank must remain empty, then disconnect the level probes and route the permeate production line to drain.

If the system needs to be powered down for more than 7 days, then the membrane housings should be filled with an appropriate preservative. The system should then be re-commissioned prior to putting back into service. See Section 8.0

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10.0 FAULT FINDING AND RECTIFICATION

Problem	Possible cause
No Power	Main fuse or supply cabling fault Pump power MCB or overload relay tripped
Power on controller motor does not run	High level probe jammed or failed Motor failure/short circuit (RED LIGHT ALERT) Power contactor/overload failure (RED LIGHT ALERT) Broken cable on contactor/overload Pump power turned off Permeate quality above limit (membrane failure)
Pump motor runs low/no production	Pump motor drive loose Concentrate valve fully open Inlet filter blocked Membrane fouled Concentrate valve fully closed
Pump cuts out during flush	Inlet filter blocked Low pressure threshold too high
Pump cuts out during service	Inlet filter blocked Water supply failure
Permeate quality reads 0	Conductivity probe disconnected/failed

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11.0 WARRANTY AND SERVICE

11.1 SERVICE

Most important. The unit must be checked and serviced by a competent professional every six months. The warranty will be invalidated if regular recorded servicing is not completed.

11.2 AFTER SALE WARRANTY Your Reverse Osmosis unit is covered by a parts warranty for a period of one year from installation on all mechanical and electrical components. Filters cartridges and membranes are excluded from this warranty since they can deteriorate due to operational or site conditions.

Should you have any problems with your Reverse Osmosis unit or require routine service, please contact your supplier.

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12.1 PROCESS AND OPERATING DATA - R/O unit

RoPro Series Reverse Osmosis Units

MODEL		8-200	8-250	8-300	8-400
PARAMETER UNITS					
Max. Output Flow*	m3/hr	10	12.5	15	20
Min Input Flow* @ 75% recovery	m3/hr	13.5	16.9	20.25	27.00
Max. Input Flow* @ 50% recovery	m3/hr	20	25	30	40
Min Cont. Flow to drain* (during service @ 75% recovery)	m3/hr	3.5	4.7	5.25	7.0
Max. Cont. Flow to drain* (during service @ 50% recovery)	m3/hr	10	12.5	15	20
Maximum Flow to drain (during flush)	m3/hr	15	21	25	35
Minimum salt Rejection %		99	99	99	99
Maximum Recovery %		75	75	75	75
Recommended Recovery %		66	75	66	66

IMPORTANT NOTES

The data quoted in the above table is affected by the inlet pressure, and so should be regarded as nominal only. * Total inlet flow and flow to drain will depend on the recovery settings chosen for the Reverse osmosis unit

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12.3 ENGINEERING DATA

RoPro Series Reverse Osmosis Units

MODEL		8-200	8-250	8-300	8-400
PARAMETER	UNITS				
Width	mm	1100	1100	1100	1100
Depth	mm	4900	4900	4900	5900
Height inc. wheels	mm	1711	1711	1711	1711
Inlet Conn.	ins	2.0	2.0	2.0	3.0
Permeate Outlet Conn.	ins	1.1/2	1.1/2	1.1/2	2.0
Drain Conn. R/O	ins	1.1/2	1.1/2	1.1/2	2.0
Delivered Wt. Kg.		600	800	900	1200
Working Wt. (approx.)	Kg.	700	1000	1100	1500
Maximum Flow to drain	m3/hr	15	21	25	35
Electrical					
Pump Power	v	415	415	415	415
	Hz	50	50	50	50
	Ph	3	3	3	3
	Rating kW	11	15	15	18.5
FLC Run	Amp	22	28	28	36

MAXIMUM INLET PRESSURE 5.5 Bar MINIMUM INLET PRESSURE 2.0 Bar MAXIMUM OPERATING TEMPERATURE 40.0C.

HEADROOM - Allow 1000 mm greater than overall height.

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12.4 PARTS DATA

Model	8-200	8-250	8-300	8-400
Frame	Stainless steel box section with angle supports			
Membrane no	Eight	Nine	Twelve	Fifteen
Membrane type	ESPA			
Membrane ref.	ESPA1 (8040)			
Pump ref.	CRN15-14	CRN20-12	CRN20-12	CRN32-9-2
Controller	OS3030			
Transformer	115 VA			
Voltage	240 - 24v			
Transformer fuses	5 A & 1A			
Power Contactor	Soft Starter			
Overload setting	22	29	29	36
Flush F/C lpm	Adjustable			
Perm flow meter	16	20	20	25
Conc flow meter	10	16	16	16
Recirc flow meter	6	6		

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13.0 EWS OS303 CONTROLLER

13.1 Manufacturers Manual

If the system has been built with an OS3030 controller, the manufacturers manual is enclosed with the system. Please refer to this for information operation and programming of the controller.

13.2 Factory programming notes

The controller has been set up with a typical operating program suitable for a reverse osmosis system of this size and type.

The programming includes a pre-service flush, post service flush, flush during service and flush during standby.

A provision has been made in the program for a 240v dosing pump to be powered during all the normal automatic service and flush operations of the system. The dosing pump outlet is not powered during the manual maintenance cycle programmed into the system because this will normally recirculate permeate that has been filled into the CIP tank.

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13.3 Factory programming

Program Step	Display	Setting	Function
1.1	Constant	0.10	Cell constant setting
1.2	Limit Min	Yes	Sets min. conductivity condition
1.3	Value Min	1.0	Sets minimum value
1.4	Switch Off	No	Not sw. off if min val. reached
1.5	Limit Max	Yes	Sets max. conductivity condition
1.6	Value Max	100.0	Set maximum value
1.7	Switch Off	Yes	Switch off is max.val. reached
1.8	Delay	60s	Delay before switching off
2.1	Temperature	25	Manual temperature comp. val.
3.1	Factor	1	Compensation correction factor
4.1		LP	Input 1 function
4.2		ST	Input 2 function
4.3		EP	Input 3 function
4.4		FU- EM- LP- EXI EP-	Function activation condition
5.1	Level Switch	1	Single level switch
5.5	Delay	10s	Low water cutout delay
5.6	Switch On	4*	Number of restarts
5.7	Delay	300s	Delay between restart attempts
5.8		PI R1I R2I R3I M- S1-	Phases when pressure monitored
5.13		PI R1I R2I R3I M- S1-	Phases when stop signal monitored
5.14	Manual Start	No	Auto start after stop signal canx
5.15	Stop Power Failure	No	Auto start after Power Failure
6.1		AP	Output 1 function Permeate Valve
6.2		MF	Output 2 function Alarm Relay
6.3		PUI IVI CVI API MFI	Output activation state
7.4	Add Program	0m	Dosing pump runs as set later
7.5	Delay	0s	Delay starting dosing output
7.9		MII MAI EM- FU-	Events triggering alarm relay
7.10		LPI ST- EPI	Events triggering alarm relay
7.11		PSI PFI MT-	Events triggering alarm relay
8.1		MII MAI EM- FU-	Events triggering alarm buzzer
8.2		LPI ST- EPI	Events triggering alarm buzzer
8.3		PSI PFI MT-	Events triggering alarm buzzer
9.1	Production 1	30s	Length of first production phase
9.2		PU- IVI CVI API	Functions active
9.3	Production 2	60s	Length of second production phase
9.4		PUI IVI CVI API	Functions active
9.5	Production 3	0s	Production phase skipped
9.7		PUI IVI CV- API	Main production phases active
10.1		IV- CV- PV-	Stop in production functions
10.2		IV- CV- PV-	Stop in rinse functions

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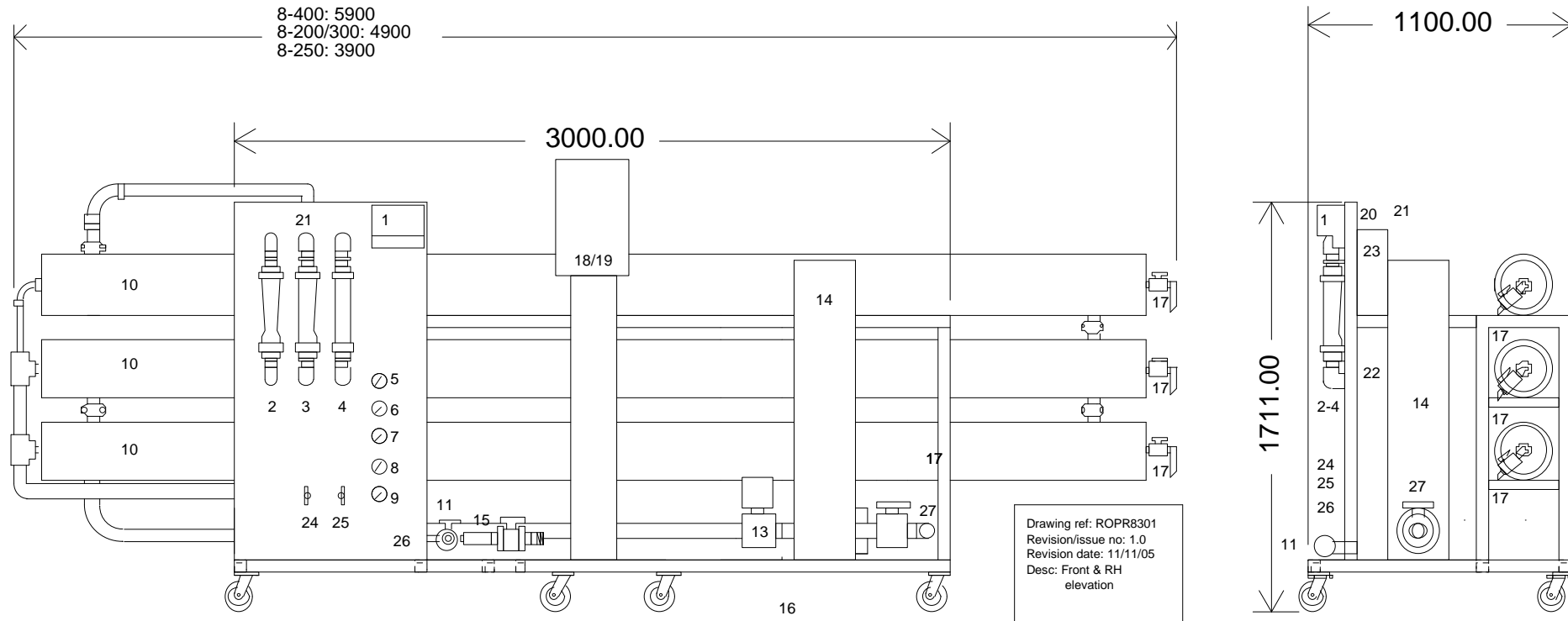
11.1		IV- CV- PV-	Stop in alarm functions
12.1	Standby	0s	Standby stage one skipped
12.3		IV- CV- PV-	Standby functions
13.1	Rinse	Yes	Rinse after production
13.2	Rinse 1	30s	Length of post production rinse 1
13.3		PU- IVI CVI API	PP rinse 1 functions
13.4	Rinse 2	180s	Length of post production rinse 2
13.5		PUI IVI CVI API	PP rinse 2 functions
13.6	Rinse 3	0s	Length of post production rinse 3
14.1	Rinse Standby	Yes	Rinse during standby
14.2	Interval	24h	Frequency of standby rinse
14.3	Rinse 1	30s	Length of standby rinse 1
14.4		PU- IVI CVI API	Standby rinse 1 functions
14.5	Rinse 2	180s	Length of standby rinse 2
14.6		PUI IVI CVI API	Standby rinse 2 functions
14.7	Rinse 3	0s	Length of standby rinse 3
15.1	Rinse Production	Yes	Rinse during production
15.2	Interval	8h	Frequency of production rinse
15.3	Rinse 1	60s	Length of production rinse 1
15.4		PUI IVI CVI API	Production rinse 1 functions
15.5	Rinse 2	0s	Length of production rinse 2
15.7	Rinse 3	0s	Length of production rinse 3
16.1	Maintenance 1	0s	Maintenance stage 1 skipped
16.3	Maintenance 2	120m	Length of maintenance st. 2
16.4		PUI IV- CV- AP-	Maintenance st. 2 functions
16.5	Interval	No	Maintenance interveal set
18.1	Code Number	No	Code number not required

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14.1 Dimension & parts identification RoPro-8 (8" membrane) Series

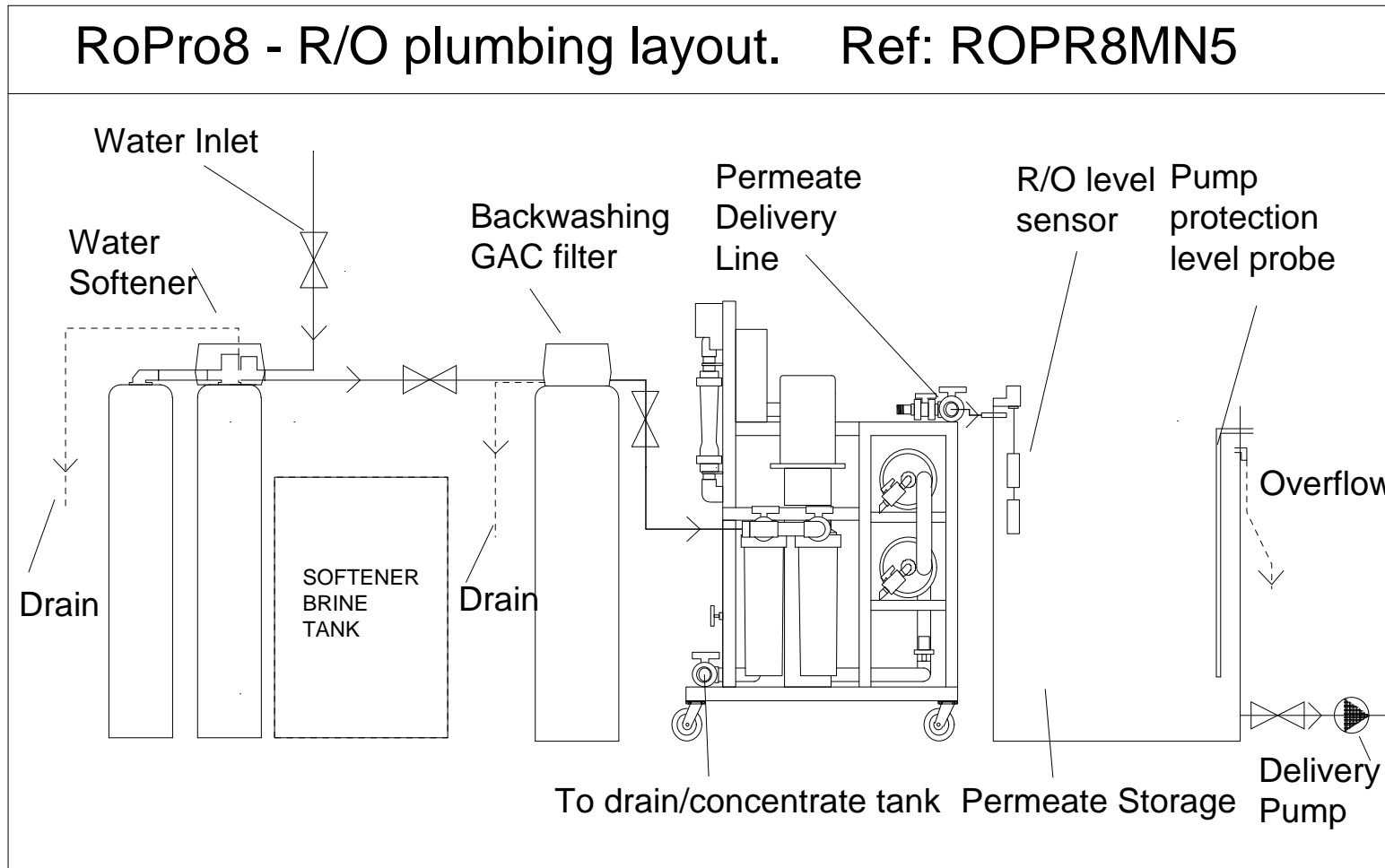
- | | | | |
|-----------------------------------|----------------------------------|---------------------------|----------------------------------|
| 1 - Controller | 8 - Inter-housing pressure gauge | 15 - High pressure switch | 22 - Conductivity probe |
| 2 - Permeate flow meter | 9 - Back pressure gauge | 16 - Low pressure switch | 23 - Pump control gear encl. |
| 3 - Concentrate flow meter | 10 - Membrane housing | 17 - Permeate sample port | 24 - Recirculation control valve |
| 4 - Recirculation flow meter | 11 - Cleaning inlet port | 18 - Pump | 25 - Pressure control valve |
| 5 - Raw inlet pressure gauge | 12 - Flush valve | 19 - Pump motor | 26 - Cleaning port outlet |
| 6 - Filtered inlet pressure gauge | 13 - Inlet valve | 20 - Permeate outlet | 27 - Raw water inlet |
| 7 - Pump pressure gauge | 14 - Sediment filter housing | 21 - Concentrate outlet | |



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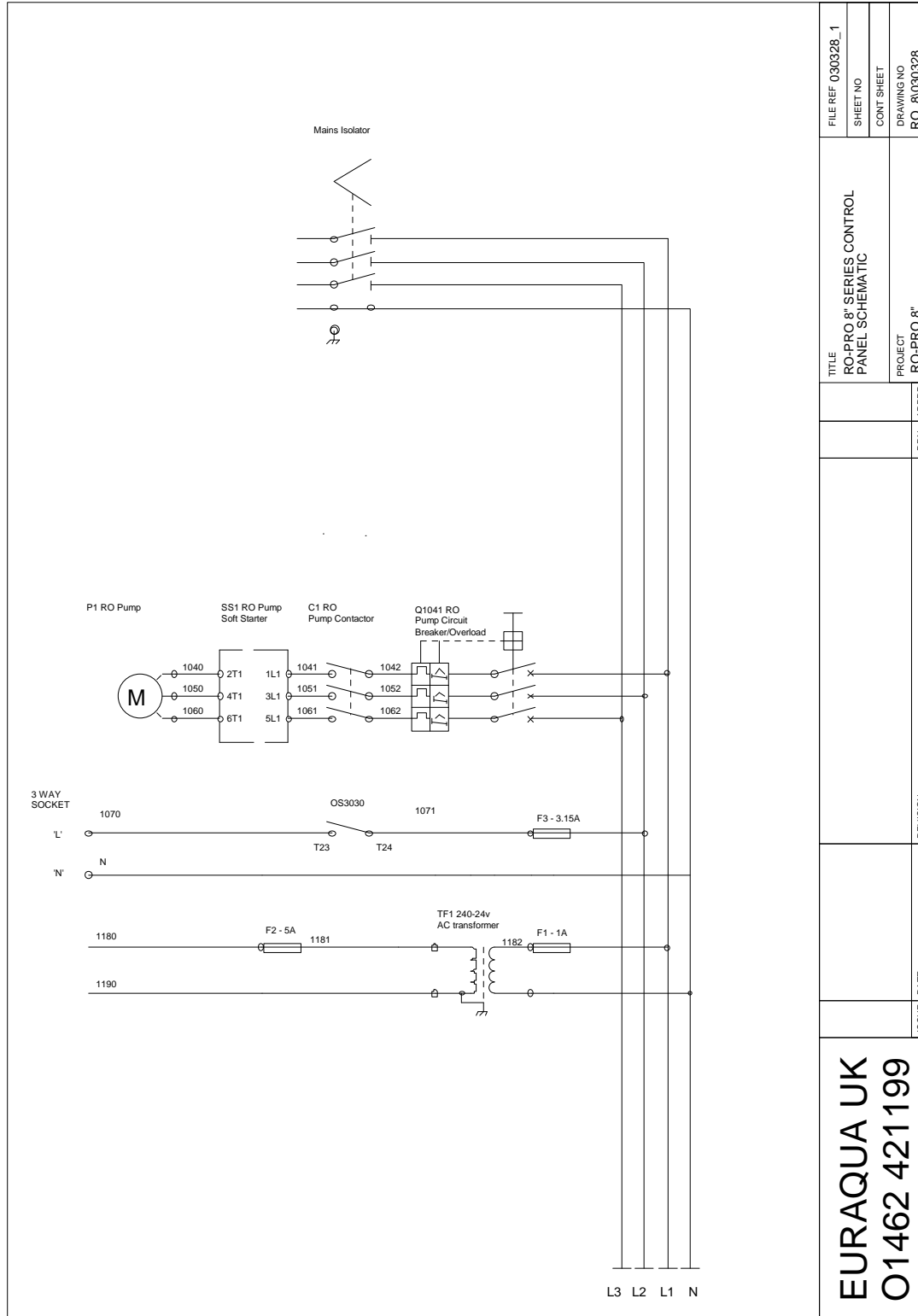
14.2 Plumbing layout



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14.3 Transformer/contactor enclosure connections OS3030

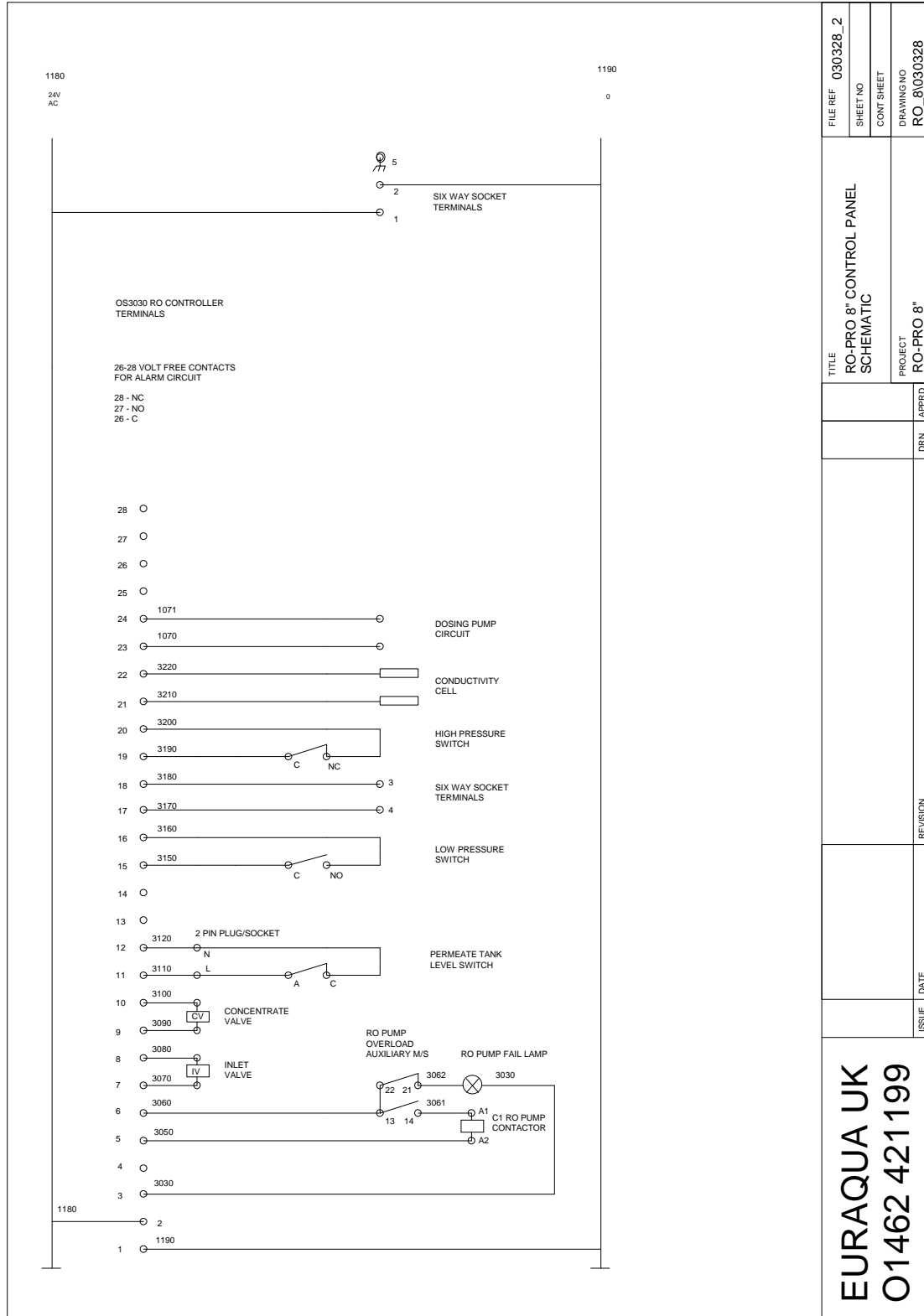


FILE REF	03032B_1
SHEET NO	
CONT SHEET	
DRAWING NO	RO_8/03032B
TITLE	RO-PRO 8" SERIES CONTROL PANEL SCHEMATIC
PROJECT	RO-PRO 8"
DRN	APPROD
REVISION	
ISSUE DATE	
EURAQUA UK 01462 421199	

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14.3 Transformer/contactor enclosure connections OS3030



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15 CE Statement

Manufacturer's Declaration of Conformity

We the undersigned

EURAQUA UK, HITCHIN, ENGLAND

Certify that the product

*type: RoPro Series Reverse Osmosis Unit
Models 8-200, 8-250, 8-300, 8-400*

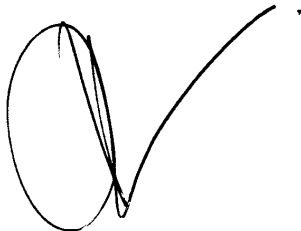
*has been designed and manufactured in accordance with the
specifications of the following:*

Directive

Machinery Directive 89/392/EEC
Low Voltage Directive 73/23/EEC
EMC-Directive 89/336/EEC

Standard

EN 292-1, EN 292-2
EN 60 335-1
EN 55 014



RT Adam
Director

Hitchin, England 01/01/05
Issue place & date